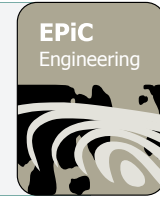




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Modelling the N₂O emissions in municipal wastewater treatment plants under dynamic conditions

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Abstract

Nitrous oxide (N₂O), a greenhouse gas with a significant global warming potential, can be produced during the biological nutrient removal in wastewater treatment plants (WWTPs). N₂O modelling under dynamic conditions is of vital importance for its mitigation. Following the activated sludge models (ASM) layout, an ASM-type model was developed considering three biological N₂O production pathways for a municipal anaerobic/anoxic/aerobic (A²/O) WWTP performing chemical oxygen demand, nitrogen and phosphorus removal. Precisely, the N₂O production pathways included were: nitrifier denitrification, hydroxylamine oxidation, and heterotrophic denitrification, with the first two linked to the ammonia oxidizing bacteria (AOB) activity. A stripping effectivity (SE) factor was used to mark the non-ideality of the stripping modelling. With the dissolved oxygen (DO) in the aerobic compartment ranging from 1.8 to 2.5 mg L⁻¹, partial nitrification and high N₂O production via nitrifier denitrification occurred. Therefore, low aeration strategies can effectively lead to a low overall carbon footprint only if complete nitrification is guaranteed. After suddenly increasing the influent ammonium load, the AOB had a greater growth compared to the NOB. N₂O hotspot was again nitrifier denitrification. Especially under concurring partial nitrification and high stripping (i.e. combination of low DO and high SEs), the highest N₂O emission factors were noted.

1 Introduction

Emissions of greenhouse gases (GHG) occur in various treatment stages during the biological nutrient removal (BNR) within wastewater treatment plants (WWTPs). Carbon dioxide (CO₂), methane (CH₄) and nitrous oxide (N₂O) are amongst these emissions (Massara, Solis, Guisasola, & Baeza, 2017). N₂O is primarily significant due to its significant global warming potential (GWP). Precisely, N₂O has a GWP 265 times higher than CO₂, in contrast to the GWP of CH₄ that is 28 times higher than the CO₂ respective one (IPCC, 2013). In this concept, the development of novel, cost-effective and flexible tools enabling the detection of GHG emissions in real time and their connection with a specific plant activity will facilitate the design of effective mitigation strategies.

The International Water Association (IWA) Activated Sludge Models (ASM) (Henze, Gujer, Mino, & van Loosdrecht, 2000) have constituted a popular mathematical tool for the description of chemical oxygen demand (COD), nitrogen (N) and phosphorus (P) removal during the BNR. Nevertheless, these models do not take account of the N₂O production and quantification.

The microbial pathways for N₂O production during the BNR in WWTPs are activated via the biochemical processes of nitrification and denitrification. The nitrification-related ones occur through the ammonia oxidizing bacteria (AOB) activity (i.e. nitrifier denitrification and hydroxylamine (NH₂OH) oxidation). Moreover, N₂O is an intermediate product of heterotrophic denitrification, which is listed as third biological pathway (Rodríguez-Caballero, Aymerich, Marques, Poch, & Pijuan, 2015; Wunderlin, Mohn, Joss, Emmenegger, & Siegrist, 2012; Wunderlin, et al., 2013; Ni & Yuan, 2015). The major parameters fostering the N₂O production have been summarized as follows: insufficient dissolved oxygen (DO) while nitrification is happening, increased nitrite (NO₂⁻) levels during both nitrification and denitrification, and low COD/N during denitrification (Kampschreur, Temmink, Kleerebezem, Jetten, & van Loosdrecht, 2009; Desloover, Vlaeminck, Clauwaert, Verstraete, & Boon, 2012; Massara, et al., 2017).

Hence, this work focused on the development of an ASM-type model that considers N₂O production in WWTPs in the most holistic way. Thus, the suggested model included N and P removal, the three biological pathways for N₂O production/consumption, N₂O stripping, and N₂O emission factor (EF) estimation under dynamic conditions (e.g. changing DO levels).

2 Materials and Methods

The model was indicatively developed for a municipal WWTP with an anaerobic-anoxic-aerobic (A²/O) configuration. The influent composition was typical of the municipal Manresa WWTP (Catalonia, Spain) (Machado, Lafuente, & Baeza, 2014). The model structure followed the IWA ASM2d principles (Henze, Gujer, Mino, & van Loosdrecht, 2000), while the microbial N₂O production pathways were described by extending and adapting relevant past studies (Pocquet, Wu, Queinnec, & Spérandio, 2016; Hiatt & Grady, 2008). Steady-state was simulated by applying constant influent composition for a period of 200 d. All the kinetic parameter values were normalized for 20 °C from the ASM2d section of Henze et al. (Henze, Gujer, Mino, & van Loosdrecht, 2000). The N₂O EF was calculated in three ways: i) N₂O-EF_{TOTAL}: considering both the stripped N₂O and the effluent N₂O (i.e. our most conservative approach), ii) N₂O-EF_{GAS}: resulting only from the N₂O stripping, and iii) N₂O-EF_{EF}: considering exclusively the N₂O released in the effluent. The N₂O stripping modelling involved the k_{L,N_2O} (i.e. the volumetric mass transfer coefficient for N₂O), as well as a factor in the range 0-1 expressing the non-ideality of the stripping modelling (i.e. stripping effectivity: SE).

3 Results and Discussion

3.1 DO effect on nitrification and N₂O emissions

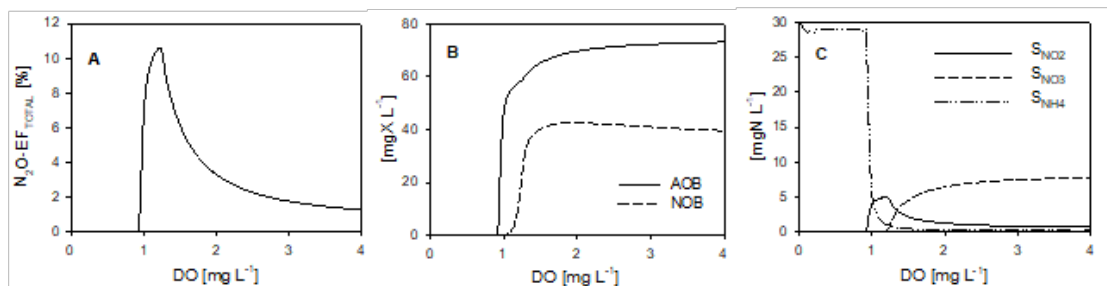


Figure 1: DO effect in the aerobic reactor on the steady state values of (A) N₂O emission factor, (B) AOB and NOB concentration, and (C) NO₂⁻, NO₃⁻ and NH₄⁺ concentrations. SE was 1.

DO ranging from 0 to 4 mg L⁻¹ in the aerobic reactor was simulated to examine the impact on nitrification and N₂O emissions. Fig. 1B and 1C show that neither AOB/nitrite oxidizing bacteria (NOB) growth, nor NO₂⁻/nitrate (NO₃⁻) production occurred under low DO (i.e. DO < 0.8 mg L⁻¹). The DO increase from 0.8 mg L⁻¹ onwards benefited the AOB growth. NOB growth started only as soon as DO rose around 1.1 mg L⁻¹ (Fig. 1B). These values (i.e. 0.8 and 1.1 mg L⁻¹) are mainly linked to oxygen affinity constants. The NOB have a lower oxygen affinity constant compared to the AOB (Wiesmann, 1994). Thus, partial nitrification/nitritation (i.e. ammonium (NH₄⁺) oxidation to NO₂⁻) strategies are designed upon the choice of a suitable DO setpoint (Guisasola, Marcelino, Lemaire, Baeza, & Yuan, 2010). In line with this, the AOB prevailed over the NOB under relatively low DO (i.e. 0.8 < DO < 1.1 mg L⁻¹) (Fig. 1B). In parallel, the NH₄⁺ concentration decreased, while NO₂⁻ started increasing. The latter can be viewed as a sign of nitritation causing NO₂⁻ accumulation (Fig. 1C). In this DO range (i.e. 0.8-1.1 mg L⁻¹), the N₂O EF significantly increased up to almost 10.5% (Fig. 1A). Under these oxygen-limiting conditions, the dominant N₂O production pathway is expected to be nitrifier denitrification. NO₂⁻ replaces oxygen at the role of the final electron acceptor and, hence, the AOB perform nitrifier denitrification (Desloover, Vlaeminck, Clauwaert, Verstraete, & Boon, 2012; Tallec, Garnier, Billen, & Gossailles, 2006; Kampschreur, et al., 2008). At a DO of 1.5 mg L⁻¹, AOB and NOB were stabilized around 70 mg L⁻¹ and 40 mg L⁻¹, respectively (Fig. 1B). (Full) nitrification began, thus leading to a continuously decreasing NO₂⁻ accumulation and a gradual deactivation of the nitrifier denitrification pathway. This can be seen in Fig. 1A by the N₂O-EF_{TOTAL} decrease that starts at a DO ≈ 1.5 mg L⁻¹ and persists with the further DO increase. Moreover, NO₃⁻ production was noted; this can be attributed to the occurrence of full nitrification (Fig. 1C). At high DO (i.e. > 3 mg L⁻¹), the N₂O EF was importantly lower (i.e. < 2%). Applying high DO (i.e. > 3 mg L⁻¹) to mitigate N₂O emissions can be effective, although quite energy-consuming. Optimizing a WWTP's operation requires the testing of various DO intervals inside which both full nitrification and moderate energy consumption are guaranteed; this can be between 1.8 and 2.5 mg L⁻¹ for the current study.

3.2 Stripping effectivity (SE) impact on the N₂O emission factor (EF)

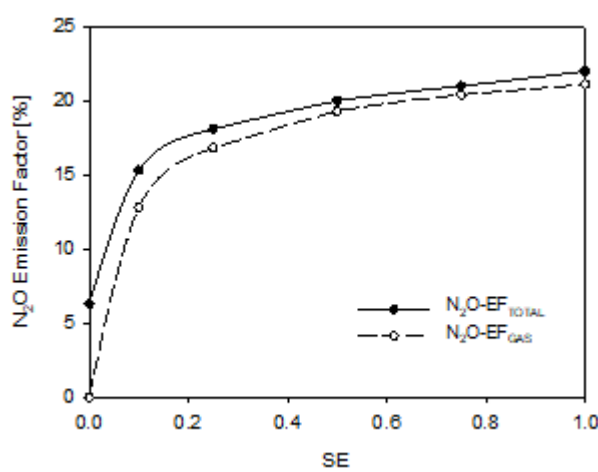


Figure 2: The maximum N₂O EF (N₂O-EF_{TOTAL}: considering both the N₂O stripped and the N₂O released in the effluent; N₂O-EF_{GAS}: referring exclusively to the N₂O stripping contribution) noted for different SE values (0, 0.1, 0.25, 0.5, 0.75, 1). Influent NH₄⁺ was 40 mg L⁻¹.

Although N₂O can be an intermediate of heterotrophic denitrification, the aerobic compartments in WWTPs (where nitrification occurs) are considered as the major N₂O hotspots. Aided by aeration, the produced N₂O is stripped and emitted to the atmosphere (Law, Ye, Pan, & Yuan, 2012; Mannina, et al., 2016). The combined effect of different DO setpoints under the highest influent NH₄⁺ value tested in this study (i.e. 40 mg L⁻¹) on the N₂O EF under different SEs (i.e. 0, 0.1, 0.25, 0.5, 0.75, 1) was examined. The results are shown in Fig. 2 for the N₂O-EF_{TOTAL} (i.e. EF considering both the stripped N₂O and the N₂O released in the effluent) as well as for the N₂O-EF_{GAS} (i.e. EF considering only the stripping contribution). Similar general trends were always noted: the maximum N₂O EF was observed at a DO ≈ 1.2 mg L⁻¹. However, the maximum absolute values were different. The maximum N₂O-EF_{GAS} ranged from 0% (SE=0) to ~21.1% (SE=1), whereas the maximum N₂O-EF_{TOTAL} from 6.3% (SE=0) to ~22% (SE=1). Thus, it can be deduced that the SE increase generally led to higher EFs (Fig. 2). The observed trend can be explained through the fact that lower SEs render the activation of the heterotrophic denitrification pathway more possible. Hence, N₂O will be rather consumed (via denitrification) than stripped. The N₂O-EF_{TOTAL} was always reported to be higher than the respective N₂O-EF_{GAS} one, although not significantly (Fig. 2). Therefore, it can be alleged that the N₂O stripping majorly contributed to the N₂O EF estimation. More importantly, the results of this study indicated that the SE factor majorly affected the final EF estimation. In this context, a more detailed stripping modelling approach is needed in the future, to avoid similar simplifications and potential EF overestimations.

3.3 Disturbing the normal WWTP operation: impact on the N₂O emission factor (EF)

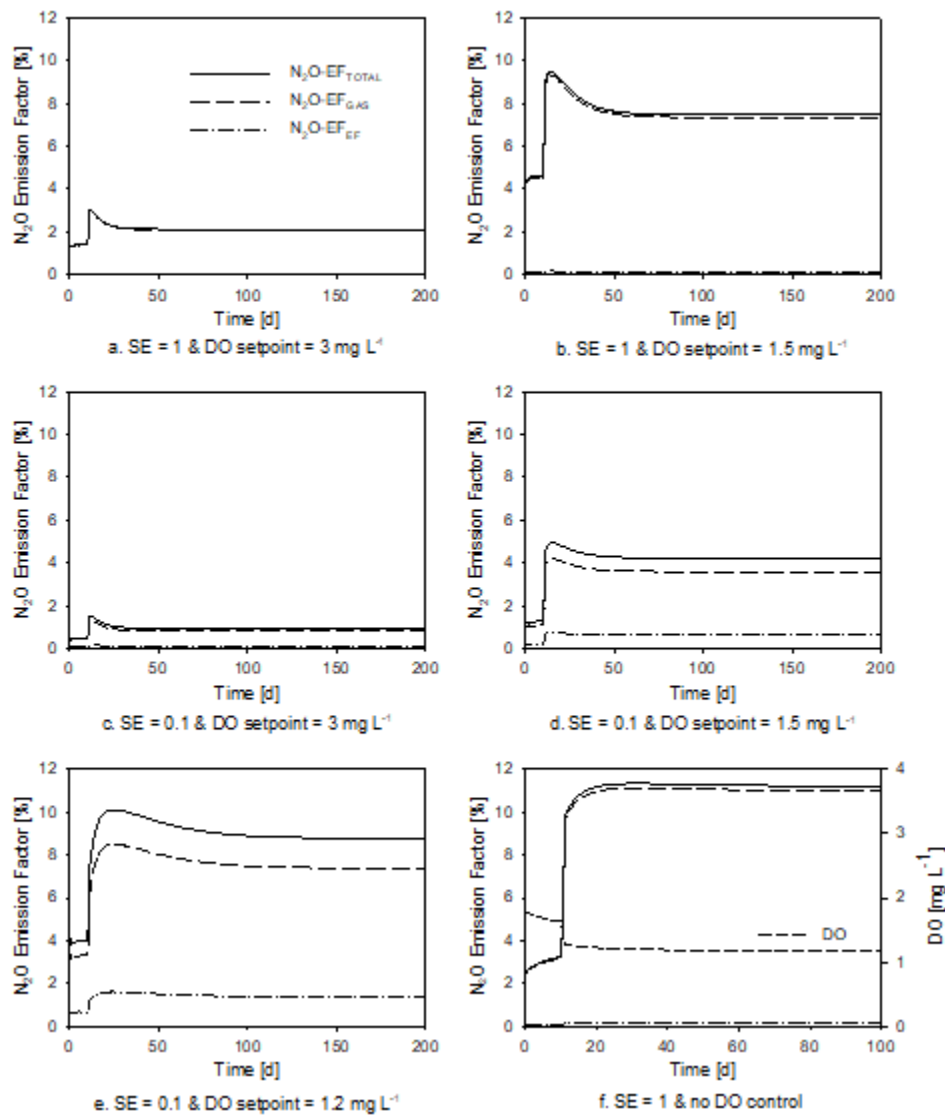


Figure 3: The effect of increasing the influent NH₄⁺ concentration (from 20 to 30 mg L⁻¹) on the 10th day of the plant operation on the N₂O EF. Different SE values (1 and 0.1) and DO setpoints (3 mg L⁻¹, 1.5 mg L⁻¹, 1.2 mg L⁻¹ and no DO control) were tested.

Transition from a system shock to normal WWTP operation creates an environment favorable to intermediates accumulation and, thus, prone to higher N₂O emissions. Within this context, the effect of a ‘step’ increase (from 20 to 30 mg L⁻¹) of the influent NH₄⁺ concentration on the 10th day of the plant operation was examined for various scenarios with different combinations of SEs and DO setpoints in the aerobic reactor. Scenarios a and b: SE was 1, thus allowing us to observe the full stripping effect. The abrupt influent NH₄⁺ increase caused a sudden increase in the N₂O emissions. The N₂O-EF_{TOTAL} ranged as follows: 1.4→3.1% almost up to the 12th day of operation (scenario a)

and 4.5→9.6% until the 17th day (scenario b). Then, the EF reduction started until it was stabilized at lower levels: at ~2.1% after the 30th day (scenario a), and at ~7.5% after the 40th day (scenario b) (Fig. 3). DO in case b was significantly lower than in scenario a; thus, higher EF values were expected. Under such conditions, the AOB perform nitritation, use NO₂⁻ as terminal electron acceptor and, finally, produce N₂O (nitrifier denitrification pathway) (Kuenen, 2008; Peng, Ni, Ye, & Yuan, 2015; Jin, Wang, & Zhang, 2016). In both scenarios a and b, the decreasing N₂O EF points to the fact that the NOB started growing and oxidizing NO₂⁻. Nevertheless, the final N₂O EF never returned to its initial value; it is possible that the NOB were not enough to oxidize all the NO₂⁻ produced. Under the same DO values, different SEs were applied to examine the effect of different levels of stripping (comparison between scenarios a and c, and comparison between scenarios b and d in Fig. 3). Decreasing the SE (from 1 to 0.1) explains the distance between the N₂O-EF_{TOTAL} and N₂O-EF_{GAS} lines. Less N₂O emissions were noted in the SE=0.1 cases (Fig. 3c and 3d); more N₂O was released in the effluent. Lowering the SE value (i.e. 0.1) decreases the stripping importance. Hence, it promotes the existence of a higher N₂O concentration inside the aerobic reactor, and the recycling of more N₂O to the anoxic reactor (where N₂O can be consumed through denitrification). Scenario e investigated the effect of DO conditions clearly harmful to the NOB growth: DO setpoint of 1.2 mg L⁻¹ and SE =0.1. N₂O emissions >9% were reported due to partial nitrification and NOB washout. Finally, scenario f indicated how the sudden influent NH₄⁺ increase effect can be more important and evident if DO is not controlled. A higher NH₄⁺ load decreases the DO concentration. Consequently, the system can shift from full to partial nitrification; the latter can explain the higher EFs noted.

3.4 Sensitivity Analysis (SA)

A local SA was performed to define the model (kinetic, stoichiometric) parameters that are mostly sensitive to the N₂O-EF_{TOTAL} at steady state. The central difference method was applied to calculate the sensitivity for each parameter. Different perturbation factors were tested within the 0.01-10% range to ensure no interference in the parameter ranking (Reichert & Vanrolleghem, 2001). As discussed in sections 3.1 and 3.3, different DO values in the aerobic reactor (i.e. varying from 1 to 4 mg L⁻¹), resulted in different EFs. In the context of understanding the cause of high N₂O emissions, the SA was conducted under two different steady-state scenarios: the 1st for a high DO setpoint in the aerobic reactor (i.e. 3 mg L⁻¹), and the 2nd for a low DO setpoint equal to 1 mg L⁻¹. The influent NH₄⁺ concentration was fixed at 30 mg L⁻¹ and the SE at 0.5. Table 1 shows the 20 most sensitive parameters to the N₂O-EF_{TOTAL} for the two applied scenarios. The values are listed in descending order considering the absolute sensitivity values. A positive sensitivity index indicates that an increase in the parameter results in increasing the N₂O-EF_{TOTAL}, while a negative sensitivity suggests the opposite. The results showed in Table 1 were obtained with a perturbation factor of 0.01% based on the study by De Pauw (De Pauw, 2005) who presented it as a factor producing equal derivative values for forward and backward differences.

The most sensitive parameters to the N₂O-EF_{TOTAL} factor varied under the two different operational modes. For the DO setpoint of 3 mg L⁻¹, the most sensitive parameters were those related to the NOB, followed by those referring to the AOB and, finally, by those related to the phosphorus accumulating organisms (PAOs). The sensitivity results for the NOB-related parameters enhance the understanding of the NO₂⁻ dynamics. The NO₂⁻ accumulation will affect the total N₂O emission factor through the activation/deactivation of the nitrifier denitrification pathway, as discussed in sections 3.1 and 3.3. Under the DO setpoint of 1 mg L⁻¹ (i.e. 2nd scenario), the AOB parameters were the most sensitive since limited NOB growth occurs in a low-DO environment (Fig. 1B). Thus, the NOB-related parameters became insensitive. For such a DO setpoint, the WWTP model performs nitritation and increased N₂O production through nitrifier denitrification is expected (section 3.1).

However, it was noted that the SE appeared only in the 17th and 20th place for the DO setpoints of 3 and 1 mg L⁻¹, respectively. The reference value of this parameter (0.5) explains the sensitivity results. According to Fig. 2, the SE parameter has a severe effect on the N₂O-EF_{TOTAL} while increasing from 0 to 0.25; its further increase from 0.25 to 1 has a lower impact on the N₂O-EF values. If a lower value had been assigned to this parameter (i.e. between 0 and 0.25), its relative sensitivity would have increased. Furthermore, Table 1 was re-examined to detect potential common parameters that appeared in the first ten places for both scenarios. It was observed that n_G (anoxic growth factor), q_{AOB_N2O_ND} (maximum N₂O production rate by the nitrifier denitrification pathway), Y_{PAO} (yield coefficient for the PAOs) and Y_H (yield coefficient for the heterotrophs) were amongst the first ten parameters for both DO setpoints; all with positive sensitivity. Hence, it can be assumed that decreasing these values leads to a decrease in the N₂O-EF_{TOTAL}. The n_G, Y_{PAO} and Y_H stoichiometric parameters, in specific, are included in the stoichiometry of the processes related to the anoxic growth of heterotrophs and PAOs. These processes can indeed significantly influence the EF since they occur in an anoxic environment where N₂O can be consumed through denitrification. Finally, the impact of the q_{AOB_N2O_ND} kinetic parameter was found to be important for both scenarios. Considering that q_{AOB_N2O_ND} expresses the N₂O production rate through nitrifier denitrification, this observation strengthens the view that nitrifier denitrification is possibly the most influential N₂O production pathway.

Table 1: Sensitivity analysis results for the two different scenarios (1st: DO_{AE} =3 mg L⁻¹; 2nd: DO_{AE} =1 mg L⁻¹); both with influent NH₄⁺ concentration=30 mg L⁻¹ and SE=0.5. DO_{AE} stands for the DO control setpoint in the aerobic reactor.

Order	DO _{AE} =3 mg L ⁻¹		DO _{AE} =1 mg L ⁻¹	
	Parameter	Sensitivity	Parameter	Sensitivity
1	Y _{NOB}	-2.138	Y _{AOB}	2.233
2	n _G	1.489	n _G	1.978
3	b _{NOB}	1.059	q _{AOB_AMO}	1.407
4	q _{AOB_N2O_ND}	0.997	Y _{PAO}	1.108
5	q _{AOB_HAO}	-0.926	b _{AOB}	-1.024
6	K _{L_O2_AOB}	0.878	n _{G5}	-0.947
7	Y _{AOB}	0.863	K _{OH5}	-0.853
8	K _{HNO2_AOB}	-0.857	q _{AOB_N2O_ND}	0.841
9	K _{NO2_NOB}	0.851	K _{O2_AOB1}	-0.738
10	Y _{PAO}	0.739	i _{NXS}	0.674
11	K _{O2_NOB}	0.629	Y _H	-0.470
12	n _{G5}	-0.620	Y _{PO4}	-0.435
13	K _{OH5}	-0.470	q _{PP}	0.400
14	K _{N2O_Den}	0.435	Y _{PAO}	-0.386
15	i _{NXS}	0.428	i _{NBM}	-0.375
16	b _{PAO}	-0.408	K _{HNO2_AOB}	-0.360
17	SE	0.375	i _{NSF}	0.338
18	Y _H	-0.364	K _{L_O2_AOB}	0.299
19	K _{MAX_P}	0.259	K _{MAX_P}	0.292

Order	DO _{AE} =3 mg L ⁻¹		DO _{AE} =1 mg L ⁻¹	
	Parameter	Sensitivity	Parameter	Sensitivity
20	i _{NBM}	-0.247	SE	0.223

4 Conclusions

An ASM-N₂O model considering COD, N and P removal, in addition to all the microbial N₂O production pathways was developed for a municipal WWTP, with emphasis on the estimation of the N₂O EF. Main conclusions:

- With the DO in the aerobic compartment ranging from 0.8 to 1.8 mg L⁻¹, high AOB growth was reported. The system moved from full to partial nitrification, thus promoting N₂O production through nitrifier denitrification. Considering the significant N₂O GWP, such operational conditions can lead to a high overall WWTP carbon footprint. Consequently, low aeration strategies can succeed only if nitrification is not disturbed.
- A SE factor (ranging from 0 to 1) was used to describe the non-ideality of the stripping modelling. Decreasing the SE meant higher N₂O concentration in the mixed liquor. The latter was translated into a higher N₂O denitrification rate inducing, subsequently, lower emissions (because of the N₂O consumption via denitrification).
- The impact of a sudden ‘step’ increase (from 20 to 30 mg L⁻¹) in the influent NH₄⁺ on the 10th day of the plant operation was studied. AOB prevailing over the NOB enhanced the NO₂⁻ accumulation and activated the nitrifier denitrification pathway. Higher emissions occurred under the following conditions: lower DO setpoints (i.e. environment more favorable to nitrifier denitrification) combined with higher SE values (i.e. higher stripping significance).
- Given the limited NOB growth under low-DO conditions (i.e. 1 mg L⁻¹), the SA showed that the NOB-related parameters had minor influence over the N₂O-EF_{TOTAL}. The n_G, q_{AOB_N2O_ND}, Y_{PAO} and Y_H parameters were amongst the top ten for both DO setpoints tested (i.e. 3 and 1 mg L⁻¹). n_G, Y_{PAO} and Y_H are related to the N₂O consumption through denitrification. q_{AOB_N2O_ND} indicates that nitrifier denitrification is possibly the most important pathway to consider for the N₂O mitigation.

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