



A Mathematical Model of Cocurrent Imbibition Phenomenon in Inclined Homogeneous Porous Medium

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Abstract

Spontaneous imbibition is the process in which the wetting phase is drawn into a porous medium by means of capillary force. Cocurrent and countercurrent spontaneous imbibitions are defined as wetting and non-wetting fluid flow in identical, and opposite directions respectively. The mathematical model is developed for cocurrent imbibition phenomenon in the inclined oil formatted homogeneous porous medium. An approximate analytical solution of the governing equation is derived by homotopy analysis method. The graphical and numerical solutions are discussed.

1 Introduction

One of the most important process in oil recovery is the spontaneous imbibition which is driven by capillary force. Such spontaneous imbibition may occur in the form of cocurrent imbibition or countercurrent imbibition. The direction of flow is the main difference between these two crucial mechanisms for imbibition. In cocurrent imbibition, the wetting and non-wetting phases flow in the same direction with the non-wetting phase being pushed out ahead of the wetting phase. In countercurrent imbibition, the wetting and non-wetting phases flow in the opposite directions. Imbibition in water-wet porous media is commonly considered as countercurrent imbibition [3, 5, 7, 13, 20, 24]. When a porous medium is partially filled with wetting phase, oil recovery is dominated by cocurrent imbibition phenomenon, not countercurrent imbibition. In the oil recovery process, cocurrent imbibition is more efficient than countercurrent imbibition [3, 20, 24].

Cocurrent imbibition phenomenon have been investigated by many authors with different viewpoints [3, 13, 20, 24]. Bourblaux and Kalaydjian [3] have discussed experimental study of cocurrent and countercurrent flows in natural porous media. Pooladi-Darvish and Firoozabadi [20] have studied the similarities and differences of cocurrent and countercurrent imbibition and pointed out the consequences for practical applications. Series solution is obtained for cocurrent imbibition during immiscible two-phase flow through porous media by Yadav and Mehta [24]. Exact integral solutions for the horizontal, unsteady flow of two viscous, incompressible fluids are derived by Mcwhorter and Sunada [13]. Homotopy perturbation method is used for solving

the problem of cocurrent and countercurrent imbibition flow into vertical porous medium by Fazeli et al. [7].

During secondary oil recovery process, it is assumed that the water is injected into fractured oil formatted inclined homogeneous porous medium and cocurrent imbibition phenomenon occurs. It is also assumed that the macroscopic behavior of fingers is governed by statistical treatment. Thus only average cross sectional area occupied by fingers is taken into account, the size and shape of individual fingers are disregarded. The velocity of oil and the velocity of water are considered under gravitational effect and inclination effect. For the investigated flow system, the porosity and permeability of inclined homogeneous porous medium are assumed to be constants. The saturation of injected water $S_w(x, t)$ is then defined as the average cross-sectional area occupied by injected water at distance x and time t .

In the current work, the mathematical model is developed for cocurrent imbibition phenomenon occurring during secondary oil recovery process. The mathematical formulation of cocurrent imbibition generates a one dimensional nonlinear partial differential equation. Homotopy analysis method is adopted to solve this equation with appropriate boundary conditions. The solution describes the saturation of injected water at distance x and time t for cocurrent imbibition phenomenon in inclined homogeneous porous medium.

2 Mathematical Modelling

2.1 Fundamental equations

During the injection process, two-phase immiscible and incompressible flow in porous medium is governed by the generalized Darcy's law for each phase as [2, 15, 21]:

$$V_w = -\frac{k_w}{\delta_w} K \left(\frac{\partial P_w}{\partial x} + \rho_w g \sin \theta \right) \quad (1)$$

$$V_o = -\frac{k_o}{\delta_o} K \left(\frac{\partial P_o}{\partial x} + \rho_o g \sin \theta \right) \quad (2)$$

where V_w and V_o are the velocities of water and oil respectively, k_w and k_o are the relative permeabilities of water and oil respectively, δ_w and δ_o are the constant viscosities of water and oil respectively, K is the permeability of the inclined homogeneous porous medium, P_w and P_o are the pressures of water and oil respectively, ρ_w and ρ_o are the constant densities of water and oil respectively, g is the acceleration due to gravity, θ is the angle of inclination with porous matrix.

The law of conservation of mass for incompressible flow gives

$$P \frac{\partial S_w}{\partial t} + \frac{\partial V_w}{\partial x} = 0 \quad (3)$$

where P is the porosity.

The sum of the velocities of injected water and native oil is the total velocity V_t in cocurrent imbibition phenomenon [9]

$$V_w + V_o = V_t \quad (4)$$

2.2 Standard relations

The difference between pressures of oil and water is defined as the capillary pressure (P_c). We assume that the capillary pressure is a function of phase saturation [19, 21]:

$$P_c(S_w) = P_o - P_w \quad (5)$$

Assume that the relationship between capillary pressure and phase saturation is of the form [14]

$$P_c(S_w) = -\beta S_w \quad (6)$$

where β is a constant.

According to Scheidegger and Johnson [22], consider the analytical relationship between relative permeability and phase saturation as

$$k_w = S_w \text{ and } k_o = 1 - \alpha S_w \quad (7)$$

where α is a constant.

2.3 Equation of motion for saturation

Combining (1), (2) and (4), we get

$$-\frac{k_w}{\delta_w} K \left(\frac{\partial P_w}{\partial x} + \rho_w g \sin \theta \right) - \frac{k_o}{\delta_o} K \left(\frac{\partial P_o}{\partial x} + \rho_o g \sin \theta \right) = V_t \quad (8)$$

Using (5) in (8)

$$\frac{k_w}{\delta_w} K \left(\frac{\partial P_w}{\partial x} + \rho_w g \sin \theta \right) + \frac{k_o}{\delta_o} K \left(\frac{\partial P_c}{\partial x} + \frac{\partial P_w}{\partial x} + \rho_o g \sin \theta \right) = -V_t \quad (9)$$

Solving (9) for $\frac{\partial P_w}{\partial x}$

$$\frac{\partial P_w}{\partial x} = - \left(K \frac{k_w}{\delta_w} + K \frac{k_o}{\delta_o} \right)^{-1} \left(K \left(\frac{k_o}{\delta_o} \rho_o + \frac{k_w}{\delta_w} \rho_w \right) g \sin \theta + K \frac{k_o}{\delta_o} \frac{\partial P_c}{\partial x} + V_t \right) \quad (10)$$

Combining (1) and (10) results in

$$V_w = -\frac{k_w}{\delta_w} \left(\frac{k_w}{\delta_w} + \frac{k_o}{\delta_o} \right)^{-1} \left(K \frac{k_o}{\delta_o} (\rho_w - \rho_o) g \sin \theta - K \frac{k_o}{\delta_o} \frac{\partial P_c}{\partial x} - V_t \right) \quad (11)$$

The pressure of water can be expressed in the form

$$P_w = \frac{P_w + P_o}{2} + \frac{P_w - P_o}{2} = \bar{P} - \frac{1}{2} P_c \quad (12)$$

where \bar{P} is the mean pressure which is constant, therefore (9) reduces to

$$K \left(\frac{k_w}{\delta_w} \rho_w + \frac{k_o}{\delta_o} \rho_o \right) g \sin \theta + \frac{K}{2} \left(\frac{k_o}{\delta_o} - \frac{k_w}{\delta_w} \right) \frac{\partial P_c}{\partial x} = -V_t \quad (13)$$

Therefore (11) implies

$$V_w = \frac{K k_w}{2 \delta_w} \frac{\partial P_c}{\partial x} - K \frac{k_w}{\delta_w} \rho_w g \sin \theta \quad (14)$$

Substituting (14) into (3), we get

$$P \frac{\partial S_w}{\partial t} + \frac{\partial}{\partial x} \left[\frac{K k_w}{2 \delta_w} \frac{\partial P_c}{\partial x} - K \frac{k_w}{\delta_w} \rho_w g \sin \theta \right] = 0 \quad (15)$$

Since $k_w = S_w$ and $P_c = -\beta S_w$, we have

$$P \frac{\partial S_w}{\partial t} - \frac{K \beta}{2 \delta_w} \frac{\partial}{\partial x} \left[S_w \frac{\partial S_w}{\partial x} \right] - \frac{K \rho_w g \sin \theta}{\delta_w} \frac{\partial S_w}{\partial x} = 0 \quad (16)$$

Using dimensionless variables

$$X = \frac{x}{L}, \quad T = \frac{\beta K t}{2 \delta_w L^2 P},$$

(16) reduces to

$$\frac{\partial S_w}{\partial T} = \frac{\partial}{\partial X} \left[S_w \frac{\partial S_w}{\partial X} \right] + A \frac{\partial S_w}{\partial X} \quad (17)$$

where $A = \frac{2L\rho_w g \sin \theta}{\beta}$ and $S_w(x, t) = S_w(X, T)$.

Eq. (17) is the nonlinear partial differential equation for the cocurrent imbibition phenomenon in the inclined homogeneous porous medium and $S_w(X, T)$ is the solution of this equation which represents the saturation of injected water at distance X and time T .

We used following boundary conditions for solving (17):

$$S_w(0, T) = 0 \text{ and } S_w(1, T) = \frac{2(1+T)}{5} \quad (18)$$

3 Solution by Homotopy Analysis Method

The homotopy analysis method which was first proposed by Liao [10, 11] is an effective and powerful technique to obtain an approximate analytical solution of nonlinear differential equation. The homotopy analysis method has been widely applied to solve nonlinear partial differential equations [4, 6, 8, 12, 16, 17, 18, 23]. Here we apply HAM to the nonlinear PDE (17). Consider the nonlinear partial differential equation

$$\mathcal{N}[\phi(X, T; q)] = 0 \quad (19)$$

where \mathcal{N} is a nonlinear operator.

We define a nonlinear operator

$$\mathcal{N}[\phi(X, T; q)] = \phi(X, T; q) \frac{\partial^2 \phi(X, T; q)}{\partial X^2} + \left\{ \frac{\partial \phi(X, T; q)}{\partial X} \right\}^2 + A \frac{\partial \phi(X, T; q)}{\partial X} - \frac{\partial \phi(X, T; q)}{\partial T}. \quad (20)$$

We choose the auxiliary linear operator

$$\mathcal{L}[\phi(X, T; q)] = \frac{\partial^2 \phi(X, T; q)}{\partial X^2}. \quad (21)$$

According to the boundary conditions (18), we choose the initial approximation of $S_w(X, T)$ as

$$S_{w_0}(X, T) = \frac{2(X^2 + TX)}{5}. \quad (22)$$

Let $q \in [0, 1]$ denote the embedding parameter, $c_0 \neq 0$ the convergence control parameter, $H(X, T) \neq 0$ an auxiliary function, \mathcal{L} an auxiliary linear operator with the property $\mathcal{L}(f) = 0$ when $f = 0$. The so-called zeroth-order deformation equation is

$$(1 - q)\mathcal{L}[\phi(X, T; q) - S_{w_0}(X, T)] = c_0 q H(X, T) \mathcal{N}[\phi(X, T; q)]. \quad (23)$$

Thus when $q = 0$ and $q = 1$, we have

$$\phi(X, T; 0) = S_{w_0}(X, T) \text{ and } \phi(X, T; 1) = S_w(X, T). \quad (24)$$

Thus $\phi(X, T; q)$ continuously deforms from the initial approximation $S_{w_0}(X, T)$ to the exact solution $S_w(X, T)$ of (17) as q increases from 0 to 1. Expanding $\phi(X, T; q)$ in Maclaurin series with respect to q , we have the homotopy-Maclaurin series

$$\phi(X, T; q) = S_{w_0}(X, T) + \sum_{m=1}^{\infty} S_{w_m}(X, T) q^m \quad (25)$$

where

$$S_{w_m}(X, T) = \frac{1}{m!} \left. \frac{\partial^m \phi(X, T; q)}{\partial q^m} \right|_{q=0} \quad (26)$$

is the m th-order homotopy derivative of $\phi(X, T; q)$. Assume that the auxiliary linear operator \mathcal{L} , the initial approximation $S_{w_0}(X, T)$, the convergence control parameter c_0 and the auxiliary function $H(X, T)$ are so properly chosen that the homotopy-Maclaurin series (25) converges at $q = 1$, we have due to (24) the homotopy series solution

$$S_w(X, T) = S_{w_0}(X, T) + \sum_{m=1}^{\infty} S_{w_m}(X, T). \quad (27)$$

Write $\overrightarrow{S_{w_n}} = \{S_{w_0}, S_{w_1}, \dots, S_{w_n}\}$. Differentiating (23) m times with respect to q , then setting $q = 0$ and finally dividing them by $m!$, we have the so-called high-order deformation equation

$$\mathcal{L}[S_{w_m}(X, T) - \chi_m S_{w_{m-1}}(X, T)] = c_0 H(X, T) \mathcal{R}_m(\overrightarrow{S_{w_{m-1}}}) \quad (28)$$

subject to the boundary conditions

$$S_{w_m}(0, T) = 0 \text{ and } S_{w_m}(1, T) = 0, \quad m \geq 1 \quad (29)$$

where

$$\chi_m = \begin{cases} 0 & \text{if } m \leq 1, \\ 1 & \text{if } m > 1 \end{cases} \quad (30)$$

and

$$\mathcal{R}_m(\overrightarrow{S_{w_{m-1}}}) = \sum_{i=0}^{m-1} S_{w_i} \frac{\partial^2 S_{w_{m-1-i}}}{\partial X^2} + \sum_{i=0}^{m-1} \frac{\partial S_{w_i}}{\partial X} \frac{\partial S_{w_{m-1-i}}}{\partial X} + A \frac{\partial S_{w_{m-1}}}{\partial X} - \frac{\partial S_{w_{m-1}}}{\partial T}, m \geq 1. \tag{31}$$

For the sake of simplicity, assume $H(X, T) = 1$. Then the solution of (28) reads

$$S_{w_m}(X, T) = \chi_m S_{w_{m-1}}(X, T) + c_0 \mathcal{L}^{-1}[\mathcal{R}_m(\overrightarrow{S_{w_{m-1}}})] + C_1 X + C_2 \tag{32}$$

where the coefficients C_1 and C_2 are determined by the boundary conditions (29). Hence

$$\begin{aligned} S_w(X, T) = & \frac{2X^2}{5} + \frac{2TX}{5} + c_0 \left(-\frac{X}{75} - \frac{2AX}{15} - \frac{4TX}{25} - \frac{ATX}{5} - \frac{2T^2X}{25} \right. \\ & + \frac{ATX^2}{5} + \frac{2T^2X^2}{25} - \frac{X^3}{15} + \frac{2AX^3}{15} + \frac{4TX^3}{25} + \left. \frac{2X^4}{25} \right) + c_0 \left[-\frac{X}{75} \right. \\ & - \frac{2AX}{15} - \frac{4TX}{25} - \frac{ATX}{5} - \frac{2T^2X}{25} + \frac{ATX^2}{5} + \frac{2T^2X^2}{25} - \frac{X^3}{15} + \frac{2AX^3}{15} \\ & + \frac{4TX^3}{25} + \frac{2X^4}{25} + c_0 \left(-\frac{7X}{375} - \frac{7AX}{750} + \frac{A^2X}{30} - \frac{TX}{75} + \frac{ATX}{25} \right. \\ & + \frac{A^2TX}{30} + \frac{AT^2X}{75} - \frac{AX^2}{150} - \frac{A^2X^2}{15} - \frac{2TX^2}{375} - \frac{2ATX^2}{15} - \frac{A^2TX^2}{10} \\ & - \frac{8T^2X^2}{125} - \frac{3AT^2X^2}{25} - \frac{4T^3X^2}{125} + \frac{8X^3}{375} - \frac{AX^3}{50} - \frac{14TX^3}{375} - \frac{2ATX^3}{25} \\ & + \frac{A^2TX^3}{15} + \frac{8AT^2X^3}{75} - \frac{4T^2X^3}{125} + \frac{4T^3X^3}{125} - \frac{AX^4}{30} + \frac{A^2X^4}{30} - \frac{TX^4}{25} \\ & \left. + \frac{13ATX^4}{75} + \frac{12T^2X^4}{125} - \frac{13X^5}{375} + \frac{26AX^5}{375} + \frac{12TX^5}{125} + \frac{4X^6}{125} \right) + \dots \tag{33} \end{aligned}$$

is an approximate analytical expression of the solution of nonlinear partial differential equation (17) which represents the saturation of cocurrent imbibition phenomenon in inclined homogeneous porous medium.

4 Results and Discussion

The convergence of homotopy analysis solution is strongly dependent on convergence control parameter c_0 . Many researchers have discussed the convergence of homotopy analysis solution using c_0 -curve; for example, Darvishi and Khani [4] have obtained series solution of the foam drainage equation, Abbasbandy et al. [1] have discussed mathematical properties of c_0 -curve in the frame work of the homotopy analysis method, Ghotbi et al. [8] have obtained the homotopy analysis solution of Richard's equation for unsaturated flow of transports in soils, Fariborzi and Naghshband [6] have discussed the convergence of homotopy analysis method to solve the Schrodinger equation with a power law nonlinearity, Patel and Desai [17] have obtained the solution of nonlinear partial differential equation of countercurrent imbibition phenomenon in inclined homogeneous porous medium.

The c_0 -curve helps us to discover the valid region of c_0 , which corresponds to the line segment almost parallel to the horizontal axis [1, 4, 6, 8, 17, 18]. The BVP1.1, a Mathematica

package [12] is used to plot the c_0 -curves. To obtain the numerical and graphical representations of the solution, we assume that the value of constants are as $L = 1$, $\rho_w = 0.1$, $g = 9.8$, $\beta = 2$.

4.1 Without inclination with porous matrix i.e. $\theta = 0^\circ$.

The homotopy analysis solution of cocurrent imbibition is derived for horizontal homogeneous porous medium and its convergence depends on c_0 which is chosen from c_0 -curve. Fig. 1 shows the c_0 -curve of $S_{w_{xx}}(0, 0)$ for 30th order approximation and $c_0 = -0.1$ is chosen from this c_0 -curve.

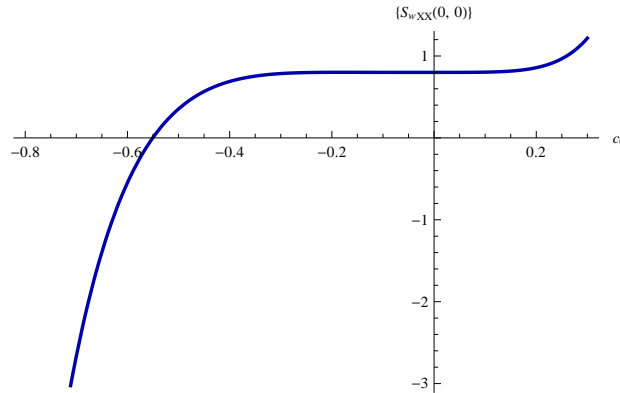


Fig. 1. The c_0 -curve of $S_{w_{xx}}(0, 0)$.

Table 1 indicates the numerical values of saturation of injected water for cocurrent imbibition phenomenon in horizontal homogeneous porous medium. The graph of saturation of injected water versus distance X for fixed time $T = 0.1, 0.2, \dots, 1$ is shown in Fig. 2.

Table 1: Numerical values of the saturation of injected water for $\theta = 0^\circ$.

T	$X = 0.1$	$X = 0.2$	$X = 0.3$	$X = 0.4$	$X = 0.5$	$X = 0.6$	$X = 0.7$	$X = 0.8$	$X = 0.9$	$X = 1$
0.1	0.0098380	0.0286652	0.0568974	0.0942209	0.1397092	0.1920183	0.2496140	0.3109845	0.3747994	0.4400000
0.2	0.0188183	0.0458898	0.0812903	0.1244648	0.1743800	0.2297261	0.2891245	0.3512995	0.4151905	0.4800000
0.3	0.0281635	0.0636062	0.1061190	0.1549784	0.2091191	0.2673299	0.3284301	0.3913983	0.4554402	0.5200000
0.4	0.0378634	0.0817849	0.1313386	0.1857117	0.2438835	0.3048009	0.3675183	0.4312809	0.4955529	0.5600000
0.5	0.0479077	0.1003971	0.1569063	0.2166188	0.2786345	0.3421151	0.4063802	0.4709492	0.5355336	0.6000000
0.6	0.0582861	0.1194149	0.1827813	0.2476568	0.3133380	0.3792522	0.4450099	0.5104064	0.5753876	0.6400000
0.7	0.0689884	0.1388107	0.2089248	0.2787865	0.3479635	0.4161957	0.4834038	0.5496570	0.6151205	0.6800000
0.8	0.0800042	0.1585579	0.2353000	0.3099718	0.3824845	0.4529325	0.5215607	0.5887067	0.6547380	0.7200000
0.9	0.0913235	0.1786304	0.2618722	0.3411796	0.4168781	0.4894526	0.5594816	0.6275619	0.6942459	0.7600000
1.0	0.1029360	0.1990029	0.2886084	0.3723799	0.4511243	0.5257485	0.5971686	0.6662294	0.7336501	0.8000000

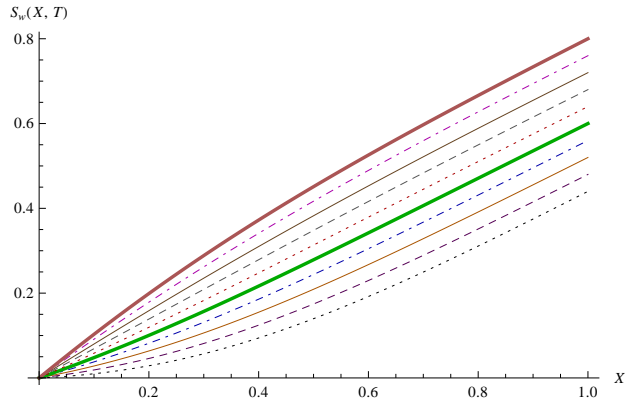


Fig. 2. Saturation of water v/s distance X for fixed time $T = 0.1, 0.2, \dots, 1$.

4.2 $\theta = 5^\circ$ inclination with porous matrix.

Fig. 3 shows the c_0 -curve of $S_{w_{XX}}(0, 0)$ for 30th order approximation and the proper value of $c_0 = -0.1$ chosen for convergent homotopy analysis solution of cocurrent imbibition in inclined ($\theta = 5^\circ$) homogeneous porous medium.

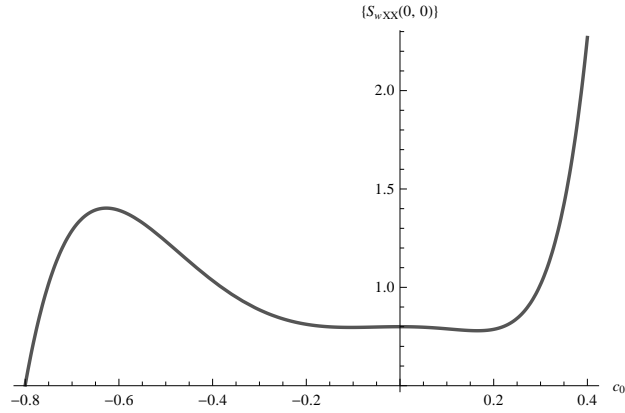


Fig. 3. The c_0 -curve of $S_{w_{XX}}(0, 0)$.

Table 2 indicates the numerical values of saturation of injected water for cocurrent imbibition phenomenon. The graph of saturation of injected water versus distance X for fixed time $T = 0.1, 0.2, \dots, 1$ is given in Fig. 4.

Table 2: Numerical values of the saturation of injected water for $\theta = 5^\circ$.

T	$X = 0.1$	$X = 0.2$	$X = 0.3$	$X = 0.4$	$X = 0.5$	$X = 0.6$	$X = 0.7$	$X = 0.8$	$X = 0.9$	$X = 1$
0.1	0.0134242	0.0353242	0.0658915	0.1046419	0.1505559	0.2022832	0.2583616	0.3174084	0.3782527	0.4400000
0.2	0.0229441	0.0533840	0.0912083	0.1357445	0.1859259	0.2404929	0.2981836	0.3578808	0.4186973	0.4800000
0.3	0.0328201	0.0719041	0.1169061	0.1670467	0.2212909	0.2785331	0.3377509	0.3981061	0.4589871	0.5200000
0.4	0.0430415	0.0908550	0.1429412	0.1985016	0.2566122	0.3163803	0.3770560	0.4380880	0.4991283	0.5600000
0.5	0.0535977	0.1102079	0.1692718	0.2300657	0.2918555	0.3540153	0.4160945	0.4778315	0.5391275	0.6000000
0.6	0.0644781	0.1299345	0.1958584	0.2616994	0.3269906	0.3914225	0.4548646	0.5173427	0.5789915	0.6400000
0.7	0.0756722	0.1500076	0.2226633	0.2933660	0.3619913	0.4285900	0.4933666	0.5566289	0.6187269	0.6800000
0.8	0.0871694	0.1704004	0.2496513	0.3250324	0.3968351	0.4655087	0.5316030	0.5956982	0.6583407	0.7200000
0.9	0.0989593	0.1910873	0.2767889	0.3566684	0.4315026	0.5021724	0.5695778	0.6345590	0.6978398	0.7600000
1.0	0.1110315	0.2120431	0.3040445	0.3882467	0.4659777	0.5385776	0.6072965	0.6732204	0.7372307	0.8000000

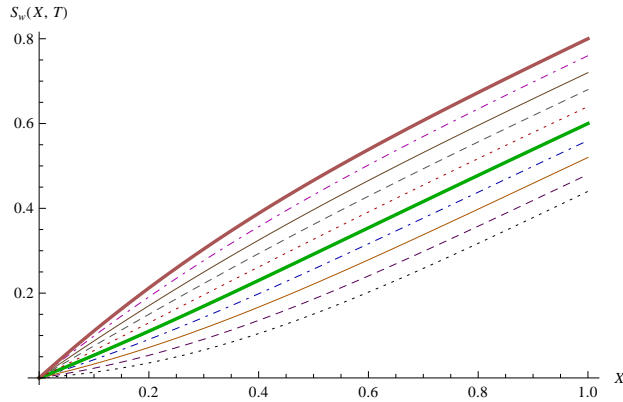


Fig. 4. Saturation of water v/s distance X for fixed time $T = 0.1, 0.2, \dots, 1$.

4.3 $\theta = 10^\circ$ inclination with porous matrix.

The homotopy analysis solution is obtained for cocurrent imbibition in inclined ($\theta = 10^\circ$) homogeneous porous medium. The c_0 -curve of $S_{w_{XX}}(0,0)$ for 30th order approximation is plotted; see Fig. 5. Here we choose proper value of $c_0 = -0.1$.

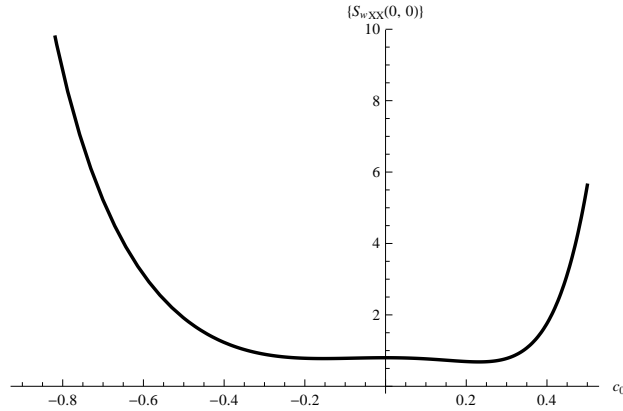


Fig. 5. The c_0 -curve of $S_{w_{XX}}(0,0)$.

The numerical values of saturation of injected water for cocurrent imbibition phenomenon are obtained (see Table 3). Fig. 6 shows the graph of saturation of injected water versus distance X for fixed time $T = 0.1, 0.2, \dots, 1$.

Table 3: Numerical values of the saturation of injected water for $\theta = 10^\circ$.

T	$X = 0.1$	$X = 0.2$	$X = 0.3$	$X = 0.4$	$X = 0.5$	$X = 0.6$	$X = 0.7$	$X = 0.8$	$X = 0.9$	$X = 1$
0.1	0.0171217	0.0421112	0.0749611	0.1150472	0.1612894	0.2123590	0.2668863	0.3236290	0.3815786	0.4400000
0.2	0.0271826	0.0609980	0.1011812	0.1469785	0.1973249	0.2510391	0.3069950	0.3642431	0.4220696	0.4800000
0.3	0.0375898	0.0803124	0.1277266	0.1790391	0.2332829	0.2894859	0.3468013	0.4045810	0.4623935	0.5200000
0.4	0.0483324	0.1000247	0.1545544	0.2111850	0.2691290	0.3276812	0.3863026	0.4446497	0.5025581	0.5600000
0.5	0.0593993	0.1201059	0.1816243	0.2433760	0.3048336	0.3656107	0.4254988	0.4844573	0.5425715	0.6000000
0.6	0.0707798	0.1405281	0.2088981	0.2755751	0.3403706	0.4032635	0.4643923	0.5240130	0.5824417	0.6400000
0.7	0.0824630	0.1612641	0.2363397	0.3077490	0.3757182	0.4406321	0.5029872	0.5633266	0.6221768	0.6800000
0.8	0.0944381	0.1822875	0.2639152	0.3398674	0.4108576	0.4777116	0.5412894	0.6024085	0.6617847	0.7200000
0.9	0.1066946	0.2035727	0.2915928	0.3719031	0.4457736	0.5144999	0.5793063	0.6412692	0.7012731	0.7600000
1.0	0.1192218	0.2250951	0.3193426	0.4038318	0.4804535	0.5509968	0.6170462	0.6799197	0.7406496	0.8000000

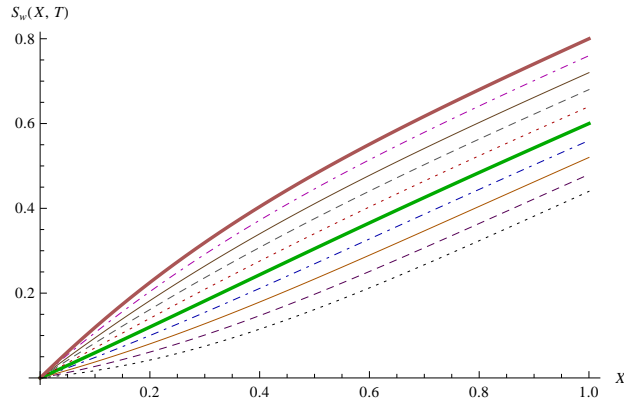


Fig. 6. Saturation of water v/s distance X for fixed time $T = 0.1, 0.2, \dots, 1$.

5 Conclusions

We have discussed cocurrent imbibition phenomenon in inclined homogeneous porous medium and its mathematical model is derived. An approximate analytical solution is obtained for cocurrent imbibition phenomenon by homotopy analysis method. The solution satisfies both the boundary conditions. The numerical and graphical interpretations are given. The saturation of injected water increases when angle of inclination with porous matrix increases. We conclude that the saturation of injected water increases when the distance increases for given time T .

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